

Claims

What is claimed is:

1 1. A fuel cell power plant (110) comprising:
2 a fuel cell stack assembly (CSA) (12) having an anode
3 region (16) having an inlet (26) and an outlet (42), a
4 cathode region (18) having an inlet (36) and an outlet
5 (46), an electrolyte region (20) intermediate the anode
6 and cathode regions, and a coolant region (22) having an
7 inlet (48) and an outlet (50); an inlet fuel stream (24)
8 operatively connected to the anode region inlet (26); an
9 inlet oxidant stream (134') operatively connected to the
10 cathode region inlet (36); a coolant loop (114)
11 operatively connected to the coolant region inlet (48)
12 and outlet (50), the coolant loop (114) including a heat
13 removal means (152, 156) for transferring heat from the
14 CSA coolant at a source temperature to a sink medium at a
15 sink temperature lower than the source temperature, the
16 difference between said source temperature and said sink
17 temperature being a temperature differential; and
18 a humidifier (70) operatively connected in the coolant
19 loop (114) and in the inlet oxidant stream (134') for
20 both cooling the coolant prior to return introduction of
21 the coolant to the CSA (12) and for relatively increasing
22 the temperature and humidity of the inlet oxidant stream
23 (134') prior to introduction of the inlet oxidant stream
24 to the CSA oxidant region inlet (36), thereby to
25 distribute the heat of at least the CSA (12) and the heat
26 removal means (152, 156) so as to increase the coolant
27 exit temperature from the CSA (12) and to the heat
28 removal means (152, 156) so as to relatively increase the
29 temperature differential between the source temperature
30 and the sink temperature.

1 2. The fuel cell power plant (110) of claim 1 wherein the
2 humidifier (70) cools the coolant sufficiently to
3 maintain the coolant inlet temperature to the CSA (12)

4 substantially constant relative to operation without the
5 humidifier (70).

1 3. The fuel cell power plant (110) of claim 1 (or 2)
2 further including a relative reduction in the size of the
3 heat removal means (152, 156).

1 4. The fuel cell power plant (110) of claim 1 (and/or 3)
2 wherein the heat removal means (152, 156) comprises a
3 radiator (152) and motorized fan (156).

1 5. The fuel cell power plant (110) of claim 1 wherein the
2 humidifier (70) comprises an energy recovery device (70)
3 for heat and mass transfer between the inlet oxidant
4 stream (134) and the coolant (114''') being returned from
5 the heat removal means (152, 156) to the CSA (12).

1 6. The fuel cell power plant (110) of claim 5 wherein the
2 energy recovery device (70) comprises a gas flow chamber
3 (72) and a liquid coolant flow chamber (74) separated by
4 a fine pore enthalpy exchange barrier (76).

1 7. The fuel cell power plant (110) of claim 5 wherein the
2 energy recovery device (70) comprises a saturator having
3 the inlet oxidant stream (134) in direct contact with the
4 coolant (114''') being returned from the heat removal
5 means (152, 156) to the CSA (12).

1 8. The fuel cell power plant (110) of claim 2 wherein the
2 heat removal means (152, 156) is of a first capacity in
3 the absence of said humidifier (70) and is of a second
4 lesser capacity in the presence of said humidifier (70).

1 9. The fuel cell power plant (110) of claim 8 wherein the
2 heat removal means (152, 156) comprises a radiator (152)
3 and motorized fan (156).

1 **10.** The fuel cell power plant (110) of claim 9 wherein
2 the humidifier (70) comprises an energy recovery device
3 (70) for heat and mass transfer between the inlet oxidant
4 stream (134) and the coolant (114''') being returned from
5 the radiator (152) to the CSA (12).

1 **11.** The fuel cell power plant (110) of claim 10 wherein
2 the energy recovery device (70) comprises a gas flow
3 chamber (72) and a liquid coolant flow chamber (74)
4 separated by a fine pore enthalpy exchange barrier (76).

1 **12.** In a fuel cell power plant (110) including
2 a fuel cell stack assembly (CSA) (12) having an anode
3 region (16) having an inlet (26) and an outlet (42), a
4 cathode region (18) having an inlet (36) and an outlet
5 (46), an electrolyte region (20) intermediate the anode
6 and cathode regions, and a coolant region (22) having an
7 inlet (48) and an outlet (50); an inlet fuel stream (24)
8 operatively connected to the anode region inlet (26); an
9 inlet oxidant stream (134') operatively connected to the
10 cathode region inlet (36); and a coolant loop (114)
11 operatively connected to the coolant region inlet (48)
12 and outlet (50), the coolant loop (114) including a heat
13 removal means (152, 156) for transferring heat from the
14 CSA coolant at a source temperature to a sink medium at a
15 sink temperature lower than the source temperature, the
16 difference between said source temperature and said sink
17 temperature being a temperature differential, the method
18 of relatively increasing said temperature differential
19 comprising the steps of:
20 cooling (74) the coolant in the coolant loop (114)
21 prior to return introduction of the coolant to the CSA
22 (12); and

23 relatively increasing the temperature and humidity
24 (72) of the inlet oxidant stream (134') prior to
25 introduction of the inlet oxidant stream to the CSA
26 oxidant region inlet (36), thereby to distribute the heat
27 of at least the CSA (12) and the heat removal means (152,
28 156) so as to increase the coolant exit temperature from
29 the CSA (12) and to the heat removal means (152, 156) so
30 as to relatively increase said temperature differential
31 between the source temperature and the sink temperature.

32 **13.** The method of claim **12** wherein the steps of cooling
33 (74) the coolant in the coolant loop (114) prior to
34 return introduction of the coolant to the CSA (12) and of
35 relatively increasing the temperature and humidity (72)
36 of the inlet oxidant stream (134') prior to introduction
37 of the inlet oxidant stream to the CSA oxidant region
38 inlet (36) comprise connecting a humidifier (70) in the
39 coolant loop (114) and in the inlet oxidant stream (134')
40 to perform both steps.